

Energy preserving multiphase flows: Application to falling films.

N. Valle*, F.X. Trias and J. Castro

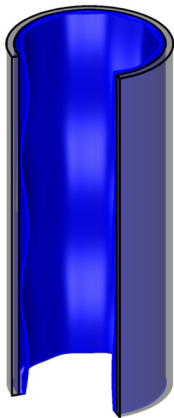
Universitat Politècnica de Catalunya - BarcelonaTech (UPC)

14th World Congress Computational Mechanics
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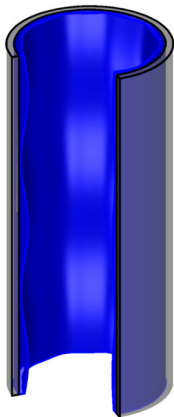
Overview

- 1 Introduction
- 2 Energy preserving
- 3 Results

Falling films in industry



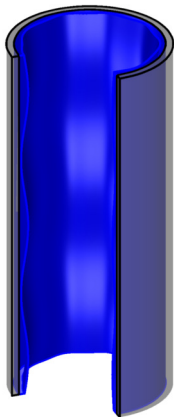
Falling films in industry



Advantages

- Short residence time

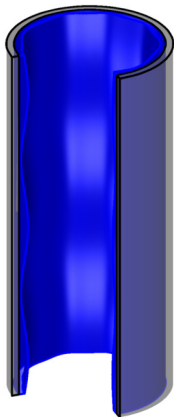
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Advantages

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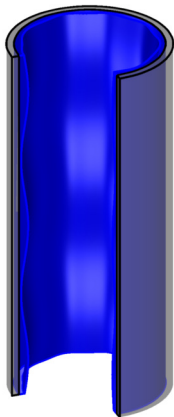
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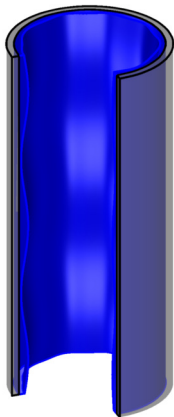
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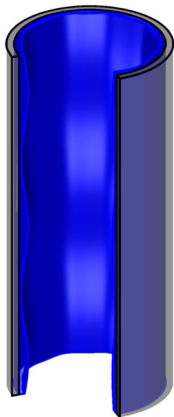
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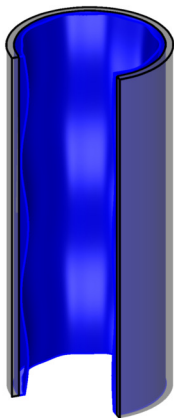
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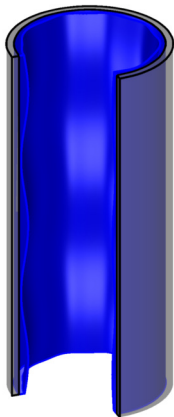
Applications

- Chemical industry
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Challenges

- Extreme density ratio

Falling films in industry



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Challenges

- Extreme density ratio
- Hydrodynamic instability at $Re = 0$

Governing equations

Incompressible

$$\nabla \cdot \vec{u} = 0$$

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Navier-Stokes

$$3\text{Re} \left(\frac{\partial (\rho \vec{u})}{\partial t} + \nabla \cdot (\rho \vec{u} \otimes \vec{u}) \right) = \nabla \cdot \sigma + \rho \hat{g}$$

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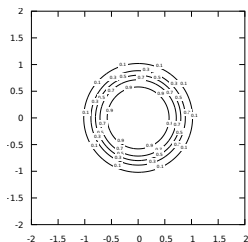
$$\sigma = \mu S - p \quad [\sigma] \hat{\eta}_i = -Wek \hat{\eta}_i$$

Regularization

$$\theta = \frac{1}{2} \left(\tanh \left(\frac{d(\vec{x})}{2\epsilon} - 1 \right) + 1 \right)$$

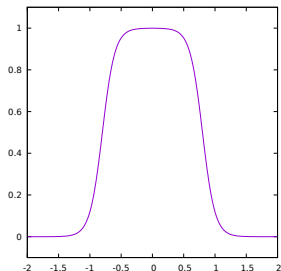
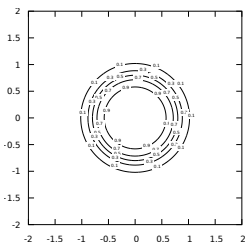
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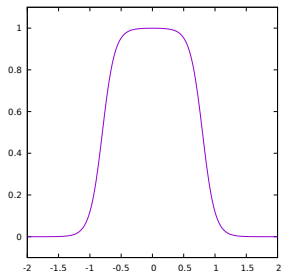
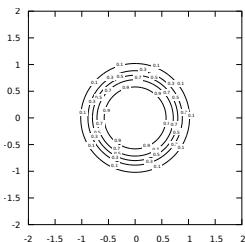
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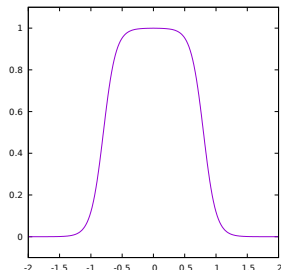
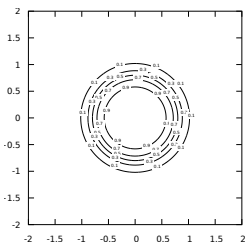
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Discrete

Conservative Level-Set

$$\frac{d\theta_c}{dt} = C(u_f)_f \theta_c$$

Navier-Stokes - Continuum Surface Force¹

$$\frac{dR_{u_f}}{dt} = -C(R_{u_f})_f u_f - G p_c + L u_f + W e k_f G \theta_c + \rho_f \hat{g}$$

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Discrete energy balance

Performing a discrete energy balance:

$$\begin{aligned} \frac{dE_k}{dt} = & - (u_f, C(Ru_f)_f u_f) - (u_f, Gp_c) + (u_f, Lu_f) \\ & + We (u_f, k_f G\theta_c) + (u_f, \rho_f \hat{g}) \\ & - \frac{1}{2} \left(u_f, u_f \Pi \frac{d\rho_c}{dt} \right) \end{aligned}$$

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$$\begin{aligned} \frac{dE_k}{dt} = & - (u_f, C(Ru_f)_f u_f) - \cancel{(u_f, G p_c)} + (u_f, L u_f) \\ & + We (u_f, k_f G \theta_c) + (u_f, \rho_f \hat{g}) \\ & - \frac{1}{2} \left(u_f, u_f \Pi \frac{d\rho_c}{dt} \right) \\ \frac{dE_p}{dt} = & We (GC(u_f)_c \theta_c, \hat{n}_f) - (u_f, \rho_f \hat{g}) \end{aligned}$$

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Consistent mass and momentum³

$$\frac{dE_m}{dt} = - (u_f, C(Ru_f)_f u_f) + (u_f, Lu_f) - \frac{1}{2} \left(u_f, U \Pi \frac{d\rho_c}{dt} \right)$$

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Consistent mass and momentum³

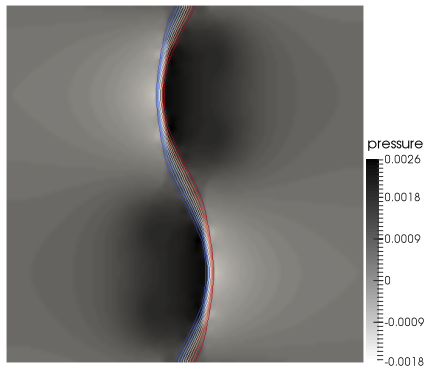
$$\begin{aligned}
 \frac{dE_m}{dt} &= - (u_f, C(Ru_f)_f u_f) + (u_f, Lu_f) - \frac{1}{2} \left(u_f, U \Pi \frac{d\rho_c}{dt} \right) \\
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 \frac{d\rho_c}{dt} &= C(u_f)_f \rho_c = D R u_f \quad \curvearrowright
 \end{aligned}$$

Energy-preserving discretization

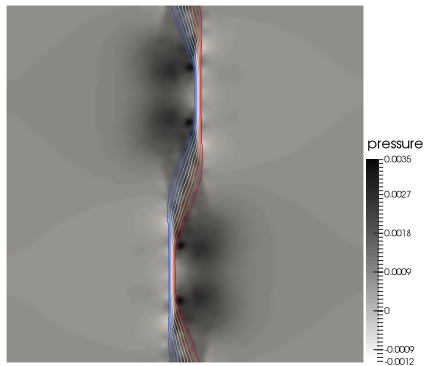
$$\frac{dE_m}{dt} = (u_f, Lu_f) < 0$$

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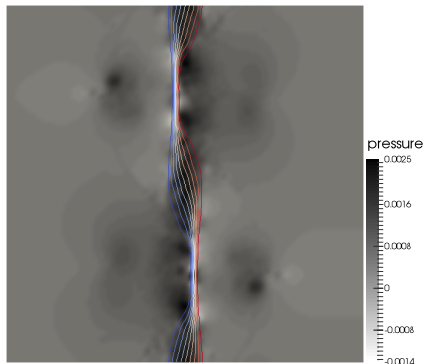
Falling Film



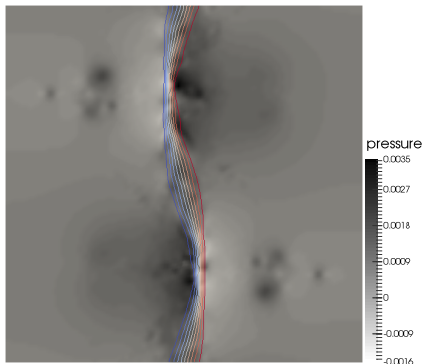
Falling Film



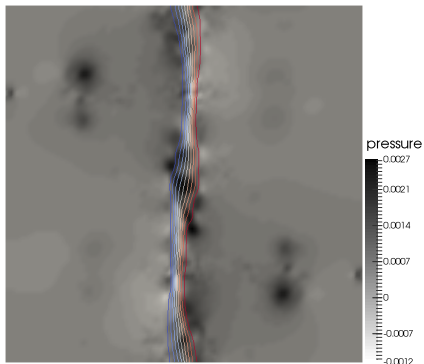
Falling Film



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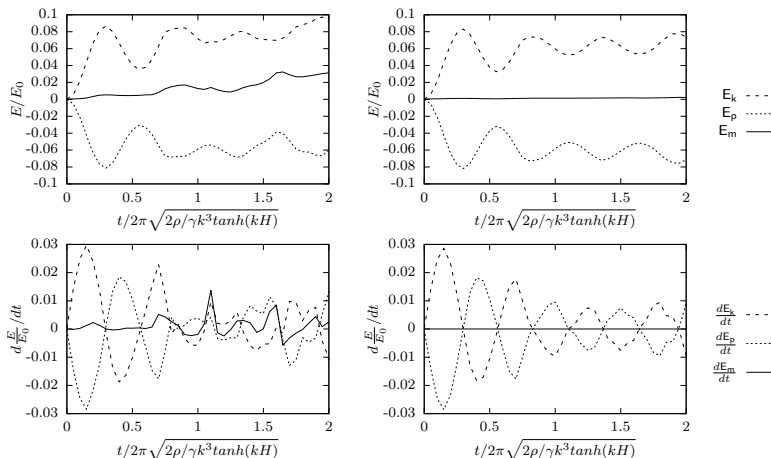


Figure: Energy fluctuation for the falling film

Simulation of industrial falling films

id	fluid	$T(^{\circ}C)$	X_{abs}	Ka	$\Pi_{\rho}(\times 10^{-3})$	$\Pi_{\mu}(\times 10^{-3})$
A	H_2O	9.9	0.00	2420	0.60	9.37
B	$H_2O/LiBr$	50.0	0.60	443	0.35	2.45
C	$H_2O/Carrol$	50.0	0.67	150	0.35	1.10

Table: Estimated fluid properties dimensionless groups. Because thermal properties are estimated at a characteristic state, values are rounded to ease its handling.

DNS of vertically falling films

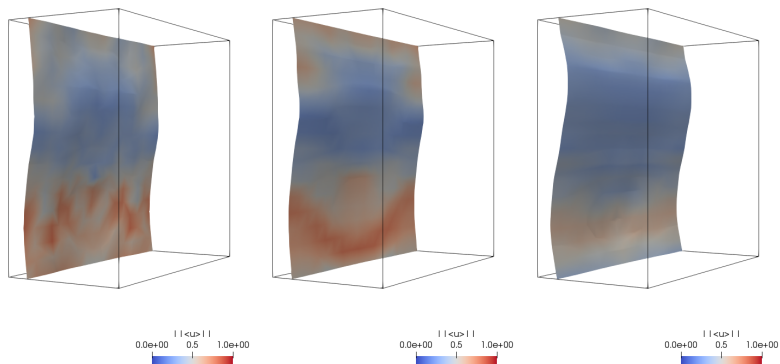


Figure: Velocity magnitude on the film surfaces for cases *A*, *B* and *C* at $Re = 150$ after $T = 100$.

Summary

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